

Chapter 4

Heat Effects

Heat Effects:

- **Sensible Heat**: When the transfer of heat produces a change in temperature.
- **Latent Heat**: When a phase change takes place with out a change in temperature.
- Other heat effects includes heat accompany **chemical reactions**, and heats associated with **formation or separation of solutions** and heat effects of **mixing process**.

4.1 Sensible Heat Effects

Molar or specific enthalpy, H ,

$$H = H(T, P)$$

Then, $dH = (\delta H / \delta T)_P dT + (\delta H / \delta p)_T dP$

C_p Eq'n(2.20) Zero, under the following conditions:

1- The change occurs @ constant pressure, $dP = 0$ Or

2- The enthalpy of substance is indep. of pressure.

(exactly for ideal gas, and approximately for low press. gases.)

Then, $dH = C_p dT$

$$\text{and} \quad \Delta H = \int_{T_1}^{T_2} C_p dT \quad (4.2)$$

Since $Q = \Delta H$ Rev., Const. Press., nonflow process & st. st. process.

$$\text{Then } Q = \Delta H = \int_{T_1}^{T_2} C_p dT \quad (4.3)$$

Similarly, $U = U(T,P)$

$$\Delta U = \int_{T_1}^{T_2} C_v dT \quad (4.1)$$

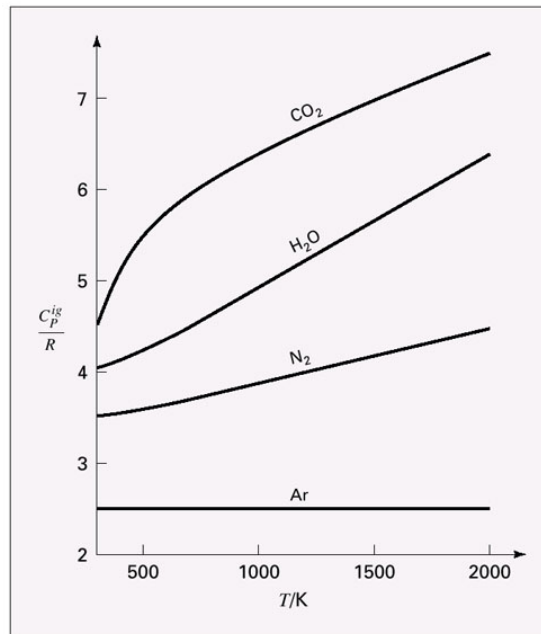
Since $Q = \Delta U$ Rev., Const. Vol., nonflow process & st. st. process.

Then $Q = \Delta U = \int_{T_1}^{T_2} C_v dT$

- **Heat Capacities of Gases**

- For gases it's the ideal gas heat capacity (rather than the actual) that is used in evaluation of the thermodynamic properties such as U and H.
- **Ideal gas** properties are used because such properties can be evaluated by two steps:
 - A. Calculation of ideal gas values from ideal heat capacities.
 - B. From PVT data of the difference between real gas and ideal gas values.
- The ideal gas heat capacities are different for different gases and **function of Temp.** but indep. of Pressure.

Figure 4.1: Ideal-gas heat capacities of argon, nitrogen, water, and carbon dioxide.



- Can be given an experimental equations:

$$C_p^{ig} = A + BT + CT^2 + DT^{-2}$$

Table C-1 gives values of these constants.
- C_p^{ig}/R is dimensionless.
- For ideal gas, $C_v^{ig}/R = C_p^{ig}/R - 1$ (4.5)
- **Heat Capacities of Gas mixtures**

$$C_{p,mixture}^{ig} = y_A C_{p,A}^{ig} + y_B C_{p,B}^{ig} + y_C C_{p,C}^{ig}$$

Where, y is mole fraction. (4.6)
- **Heat Capacities of solids & liquids**

$$C_p/R = A + BT + CT^2 + DT^{-2}$$

Table C-2, C-3 and Perry's hand book, gives values of these constants.

Read Ex. 4.1 and 4.2

- Iteration procedure is required to calculate T_2 given T_1 and Q or ΔH .

- Define a mean heat capacity, C_{P_H} , as

$$C_{P_H} = \int_{T_1}^{T_2} C_p dT / (T_2 - T_1)$$

- Substitute to the above eq'n,
 $C_p / R = A + BT + C T^2 + DT^{-2}$
 and integrate,

$$C_{P_H} / R = A + BT_H + C/3 (4 T_H^2 - T_1 T_2) + D / T_1 T_2$$

a

Where $T_H = (T_1 + T_2) / 2$ The arithmetic mean temperature.

- Then, $\int_{T_1}^{T_2} C_p dT = C_{P_H} (T_2 - T_1)$

and,

$$\Delta H = C_{P_H} (T_2 - T_1)$$

b

Consequently,

$$T_2 = \Delta H / C_{P_H} + T_1$$

c

Solve by iteration:

- Assume value of T_2 .
- Subs. in eq'n **a**, then find C_{P_H} .
- Subs. in eq'n **c**, then find T_2 .
- Recalculate C_{P_H} , repeat until convergence is achieved for T_2 .

OR, use the book solution using τ

4.2 Latent Heats of Pure Substances

- Latent heat of
Fusion $S \rightarrow L$
Vaporization $L \rightarrow G$
Sublimation $S \rightarrow G$

During this process, 2 phases exist.

- Latent heat is function of temp. and related to other system properties by exact thermodynamic equations:

Clapeyron Equation

$$\Delta H = T \Delta V dp^{\text{sat}}/dT \quad (4.11)$$

Where,

ΔH = Latent heat.

ΔV = Volume change accompanying the phase change.

p^{sat} = Vapor pressure.

When applied for vaporization,

dp^{sat}/dT = Slope of vapor pressure vs. temp.

$$\Delta V = V_{\text{vap}}^{\text{sat}} - V_{\text{liq}}^{\text{sat}}$$

- Latent heats may also be measured calorimetrically. Experimental values are available at selected temperatures for many substances.
- Correlations, like Clapeyron, are available but not enough data information at the desired temperature are known.
- For this reason, approximate methods have been developed to estimate latent heat of vaporization. They serve one of two purposes:
 - To predict the heat of vaporization at the normal boiling point.
 - To estimate the heat of vaporization at any temperature from that known at another single temperature.

- ❖ **Trouton's rule:** Rough estimates of latent heat of vaporization for pure liquids at their normal boiling point.

$$\Delta H_n / R T_n \sim 10$$

Experimental values for this ratio are: Ar, 8.0; N₂, 8.7; O₂, 9.1; HCl, 10.4; C₆H₆, 10.5; H₂S, 10.6; and H₂O, 13.1.

- ❖ **Riedel Equation:**

$$\Delta H_n / R T_n = 1.092 (\ln P_c - 1.013) / 0.93 - T_{r_n} \quad (4.12)$$

Where, T_n = normal boiling pt.

ΔH_n = molar latent heat of vaporization @ T_n.

P_c = critical pressure, bar.

T_{r_n} = reduced temp. @ T_n.

Error < 5%

- ❖ **Watson Equation:**

$$\Delta H_2 / \Delta H_1 = (1 - T_{r_2} / 1 - T_{r_1})^{0.38} \quad (4.13)$$

Simple and accurate.

Read Ex. 4.4

4.3 Standard Heat of Reaction

- Chemical reactions are accompanied by the transfer of heat, by temp. changes or by both.

- Enthalpy changes during reaction

$$\Delta H = \Delta H_p - \Delta H_R$$

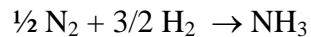
Or the heat of reaction, when both reactant and products are under the same T, P.

- Standard states:

- Liquids and solids: The real pure liquid or solid at 1 bar.
- Gases: The pure substance in the ideal-gas state at 1 bar (10^5 Pa). (used to be 1 atm (101,325 Pa)).

- Property values at standard state is denoted by (^o). For example heat capacity at standard state is: $C_p^o = C_p^{ig}$

- The heat of reaction depends on how the reaction written:



$$\Delta H_{298}^o = -46,11 \text{ J}$$

Or



$$\Delta H_{298}^o = -92,22 \text{ J} \quad (\text{Double})$$

4.4 Standard Heat of Formation

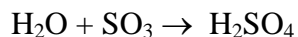
- *A formation reaction is the reaction, which forms one mole of a single compound from its constituent elements.*

For example,



The formation reaction of Methanol.

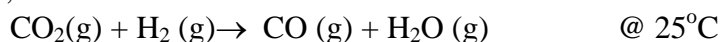
But,



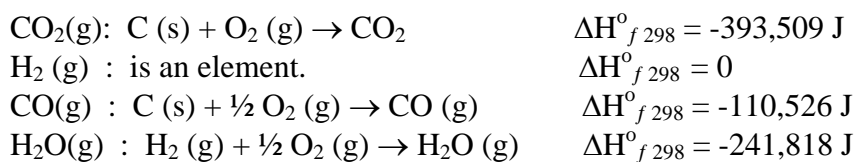
Not formation reaction.

- The standard heat of formation for compounds are tabulated at 298 K (the standard reference temperature). (ΔH°_{298}).
Given at table C.4.
- Heat of formation reactions at different temperatures can be calculated from heat capacity data and the known value of the standard heat of formation at 298 K.
- **Standard heat of formation for any elements = 0.**
- Chemical equations and standard heat of reaction resulted may added or subtracted to give the standard heat of the required reaction. (Hess's law).

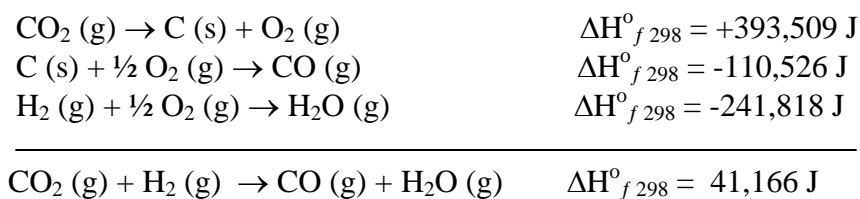
Consider,



The formation reactions related to this reaction are as follow:



Rewrite these equations so that their sum gives the desired reaction



- Standard heat of formation depend on the compound state (g, L, ...).



However, for



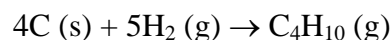
The difference (44,012 J) is approximately the heat of vaporization of H_2O @ 25°C .

Read Example 4.5

4.5 Standard Heat of Combustion

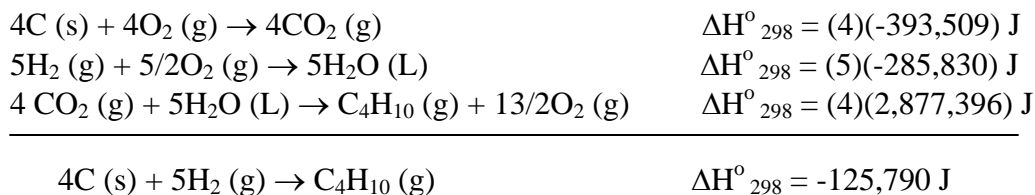
- A combustion reaction is defined as a reaction between an element or compound and oxygen to form specified combustion products.**
- Many standard heat of formation can be determined through combustion reactions.

Consider the formation of n-butane



This reaction does not proceed as indicated above.

So, we can't directly measure its heat of formation. However consider the combustion reactions:



The result is standard heat of formation of n-butane listed in table C.4.

4.6 Temperature Dependence of ΔH°

- Standard heat of reaction from standard heat of formation at 298 K can be calculated directly:

$$\Delta H^\circ = \sum \nu_i \Delta H_{f,i}^\circ \quad (4.15)$$

For example, $4\text{HCl (g)} + \text{O}_2 \text{ (g)} \rightarrow 2\text{H}_2\text{O (g)} + 2\text{Cl}_2 \text{ (g)}$

$$\Delta H^\circ = 2 \Delta H_{f,\text{H}_2\text{O}}^\circ - 4 \Delta H_{f,\text{HCl}}^\circ$$

@ 298 K from table C.4

$$\begin{aligned} \Delta H^\circ &= 2(-241,818) - 4(-92,307) \\ &= -114,408 \text{ J} \end{aligned}$$

- If reaction occurs at temperature other than 298 K,

$$d \Delta H^\circ = \Delta C_p^\circ dT \quad (4.17)$$

Integrate between 298K and T

$$\Delta H^\circ = \Delta H_{298}^\circ + R \int_{298.15}^T \Delta C_p^\circ / R dT \quad (4.18)$$

Then,

$$\Delta H^\circ = \Delta H_{298}^\circ + \Delta C_{p,H}^\circ (T - 298.15)$$

Where $\Delta C_{p,H}^\circ$ can be evaluated similar to $C_{p,H}^\circ$ (mean heat capacity) as:

$$\Delta C_{p,H}^\circ / R = \Delta A + \Delta B T_H + \Delta C / 3 (4 T_H^2 - T_1 T_2) + \Delta D / T_1 T_2$$

Where $\Delta A = \sum \nu_i A_i$ and so on

Read Example 4.6.

4.7 Heat Effects Of Industrial Reactions

- Industrial reactions are rarely carried out under standard state conditions.
 - Reactants may not present in stoichiometric ratios.
 - Reaction may not go to completion.
 - Final temperature may differ from the initial temperature.
 - Inert species may be present.
 - Several reactions may occur simultaneously.
- Calculations of the heat effects of actual reactions are based on theoretical flame temperature (TFT) calculation.
- TFT: is useful to predict the highest achievable temperature, which is useful to select the material type. Usually highest temperature occurs at adiabatic process.

Example 4.7

Read Examples 4.8 and 4.9